ASIAN PAINTS LTD PENTA DIVISION, CUDDALORE - TAMILNADU

24TH NATIONAL AWARD EXCELLENCE IN ENERGY MANAGEMENT 2023

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ASIAN PAINTS LTD PENTA DIVISION, CUDDALORE -TAMILNADU



TEAM MEMBERS

SAMPATHKUMAR – Senior Manager – Plant Engineering
 ALKESH MODI – Manager – Plant Engineering
 M.ARUNKUMAR – Asst. Manager – Technical Services



ABOUT OUR GROUP

#1 Paint company in India



80+ YEARS OF DELIVERING

A JOY

42 Beautiful home stores in India

27 In house paint

manufacturing

facilities worldwide

240+ scientists driving innovation

60+ Countries

served

1,730,000 Installed in-house decorative paint manufacturing capacity in India (KL per annum)



PROTECTIVE, PERFORMANCE AND POWDER COATINGS

Weatherscol

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ADISCO Opasianpaints



PAINT MANUFACTURING LOCATIONS IN INDIA# (Installed capacity/annum)

Decorative coatings

Rohtak, Haryana 400,000 KL Kasna, Uttar Pradesh 80,000 KL Ankleshwar, Gujarat 130,000 KL Khandala, Maharashtra 300,000 KL Patancheru, Telangana 80,000 KL Visakhapatnam, Andhra Pradesh 300,000 KL Mysuru, Karnataka 300,000 KL Sriperumbudur, Tamil Nadu 140,000 KL Chemical

Cuddalore, Tamil Nadu 8,760 MT*

Industrial Coatings

Sarigam, Gujarat (Facility of subsidiary company) 7,200 MT

Taloja, Maharashtra 14,000 KL

ASIAN PAINTS LTD PENTA DIVISION



- Asian paints Ltd Penta Division Manufactures Specialty Grades chemical for the past 36 years.
- Producing Various grades of Pentaerythritol
 - 1. Tech Pentaerythritol
 - 2. Mono Pentaerythritol
 - 3. Di Pentaerythritol
 - 4. Sodium formate
- Catering to Alkyd resin, Aircraft specialty lubricant additive, PVC stabilizers, Explosives, Leather Tanning and Oil drilling industries
- Pentaerythritol 876
 Sodium formate 525

- 8760 MT , - 5250 MT.

• ISO14001, ISO 9001 & ISO 45001 Certified



PROCESS FLOW -PENTAERYTHRITOL











SPECIFIC STEAM CONSUMPTION (MT / MT PRODUCT)



SP.STEAM CONSUMPTION



SPECIFIC POWER CONSUMPTION (KWH / MT OF PRODUCT)



POWER CONSUMPTION KWH/TON



YEAR	NUMBER OF ENERGY SAVINGS PROJECT	INVESTMENT (INR MILLION)	ELECTRICAL SAVINGS (MILLION KWH)	THERMAL SAVINGS (MILLION KCAL)	TOTAL SAVINGS (INR MILLION)	PAYBACK PERIOD IN MONTHS
FY 2020 -21	3	4.569	0.003	302	5.265	10
FY 2021 -22	5	10.26	0.042	3355	4.663	26
FY 2022 -23	9	1.49	0.088	12065	16.385	1





YEAR	NAME OF ENERGY SAVINGS PROJECT	INV (INR LAKHS)	ELECTRICAL SAVINGS (KW /ANNUM)	THERMAL SAVINGS (TONS/ANNUM)	TOTAL SAVINGS (LAKHS/ANNUM)	PAYBACK PERIOD IN MONTHS
2020-21	Stripper Reboiler converted from Plate heat exchanger to Shell and Tube type	45	_	3974	63.59	14
2020-21	Di Dryer debottlenecking	1	-	1296	20.736	0.5
2020-21	Replacement of 125W MV lamp with 60W LED fitting (10 Nos.) in Fa, Methanol and Aa bullet area	0.6	2847	-	0.18	40

ENERGY SAVINGS PROJECT IMPLEMENTED IN FY 2021-22



YEAR	NAME OF ENERGY SAVINGS PROJECT	INV (INR LAKHS)	ELECTRICAL SAVINGS (KWH/ANNUM)	THERMAL SAVINGS (TONS/ANNU M)	TOTAL SAVINGS (LAKHS/AN NUM)	PAYBACK PERION IN MONTHS
2021-22	Stripper Packing Height increased from 10 m to 11.3 m in the Existing stripper column	10	-	4320	69	2
2021-22	Provision of VFD for M-206 agitator and speed reduced from 50Hz to 30Hz	0.44	11520	-	0.70	8
2021-22	Replacement of standard motor to IE3 motor 5 nos. (P-106-D 5HP, P-180 3HP, P-133 5HP, P-181-2 7.5HP, P- 201-1 3HP	1.03	15360	-	0.97	13
2021-22	Replacement of 125W MV lamp with 60W LED fitting (10 Nos.) in Aa bullet area	0.6	2847	-	0.18	40
2021-22	Replacement of 165W SV lamp with 30W LED fitting in pole light (20Nos.)	0.55	11826	-	0.75	9

ENERGY SAVINGS PROJECT IMPLEMENTED IN FY 2022-23



YEAR	NAME OF ENERGY SAVINGS PROJECT	INV (INR LAKHS)	ELECTRICAL SAVINGS (KWH/ANN UM)	THERMAL SAVINGS (TONS/ANNUM)	TOTAL SAVINGS (LAKHS/AN NUM)	PAYBACK PERION IN MONTHS
2022-23	Reduction of Water input by changing the Reaction Formulation	0.5	-	10134	162	1
2022-23	Automation of Fresh water input to the CBF cake tank	1.10	-	1140	18.24	1
2022-23	Heat recovery from the Stripper Vapor	6	-	1339	21.42	4
2022-23	Heat recovery from the DEE distillate	0.1	-	475	7.6	1
2022-23	Provision of transparent roof sheet in coal yard and Lighting circuit separation	1.7	6132	-	0.41	50

ENERGY SAVINGS PROJECT IMPLEMENTED IN FY 2022-23



YEAR	NAME OF ENERGY SAVINGS PROJECT	INV (INR LAKHS)	ELECTRICAL SAVINGS (KWH)	THERMAL SAVINGS (MILLION KCAL)	TOTAL SAVINGS (LAKHS/AN NUM)	PAYBACK PERION IN MONTHS
2022-23	Replacement of CT pump P-1610-B 75KW motor to 52KW motor	0.05	3840	-	0.25	3
2022-23	Replacement of standard motor 52KW to 30KW IE2 motor Off gas blower	0.1	11520	-	0.78	2
2022-23	Provision of VFD for CT fan 2 with temperature-based running	0.2	23040	-	1.56	2
2022-23	Provision of separate energy meter for monitoring and air leakage arresting	0.2	49920	_	3.34	1



INTERNAL BENCHMARK

Target Vs Actual





MAJOR ENCON PROJECTS PLANNED FY 23-24



Steam Header Augmentation

Elimination of High-pressure steam consumption in Process



Investment:

• 100 Lakh

Benefits:

- Generation of 84 Kwh
- Steam saving 4 TPD

Separate Pump for high head condenser

Provision of separate high efficiency pump for high head condenser



Investment:

• 20 Lakh

Benefits:

• Generation of 30 Kwh

Distillation column feed location optimization

Distillation column internal packing's structure will be changed based on feed



Investment:

• 12 Lakh

Benefits:

- Steam Savings 3.6 TPD
- Generation of 0.2 Kwh

INNOVATIVE PROJECTS

- 1. Changes made in Raw material addition in Reactor based on Reaction Chemistry study to increase the yield
- 2. Stripper Debottlenecking
- 3. Stripper Reboiler Conversion





INNOVATIVE PROJECT 1





WATER INPUT TO SYSTEM 11214 KGS

WHY THE PROJECT IS INNOVATIVE ?

- Aldol Condensation reaction when the Aldehyde concentration decreases the Product yield will increase
- Le chatelier Principle "Changes in the temperature, pressure, volume, or concentration of a system will result in predictable and opposing changes in the system in order to achieve a new equilibrium state".
- Maintaining the low aldehyde concentration throughout the reaction by changing the Reactant 1 addition increases the Product yield
- Increase in End temperature by 13 degC leads to opposing changes I,e. conversion of impurities into Desirable Product
- Reaction output Total solids increased by 14%
- Resulting into reduction in steam requirement in the downstream process.





REACTION STEPS (Original Vs Modified)

NEW REACTION 38 MIN RM ADDITION PATTERN (PERCENTAGE ADDITION / MIN)



REACTION STEPS (Modified)





REDUCTION IN WATER PER BATCH 1627 KGS





SECTION	UNIT	STEAM REQUIREMENT IN ORIGINAL REACTION FORMULATION	STEAM REQUIREMENT IN MODIFIED REACTION FORMULATION
STRIPPER	Kg/Hr	6560	5750
DISTILLATION COLUMN	KG/HR	800	700
EVAPORATOR	KG/HR	2100	1800
TOTAL STEAM	KG/HR	9460	8250
STEAM SAVINGS	KG/HR	12	210



INNOVATION 2 STRIPPER DEBOTTLENECKING





Theory of Constraints: Steps

• Goldratt's Five Steps

- 1. Identify the systems constraints
- Decide how to exploit the constraints Get the most
- 3. Subordinate everything else to the exploitation of constraints Treat the constraint as a king.
- 4. (Evaluate various alternatives to) Elevate the systems constraint -spend more money to make more money
- 5. If in the previous steps , A constrain has been broken go back to Step 1 repeat the process



INNOVATIVE 2 – STRIPPER DEBOTTLENECKING



• PROJECT DETAILS

"Achieve the intended purity in Stripper column by increasing the packing height in the empty space available in the existing column"



WHY THE PROJECT IS INNOVATIVE

- Stripper column is the Major Steam consumption equipment in our Process
- The Purpose of the stripper is to remove the excess Reactant from Reactor output.
- The stripper column was designed to operate with 40% evaporation rate to achieve the bottom purity, i.e., <0.1% Aldehyde in the stripper bottom

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- To maximize the throughput, The stripper operated at its fullest capacity (I,e. 13000 kg/hr feed and 6700 kg/hr steam), but due to capacity limitation even at increased evaporation rate of 44%, achieved bottom purity of 0.12%.
- To achieve the purity ,reduce the steam consumption and to increase the throughput we increased the packing height of 1.3 m in the existing stripper column in the available space with no major investment.

INNOVATIVE 2 – BENIFITS OF THE PROJECT



S:NO	OPERATING PARAMETERS	BEFORE	AFTER	SAVINGS
1	Feed rate maximum	13000 kg/hr.	13000 Kg/hr.	
2	Evaporation Rate	44%	40%	
3	Steam flow Kg/hr	6700	6135	565 kg/hr.
4	Stripper Bottom quality	0.12 % Fa	0.05 % fa	

Note: Innovation 2 gives the additional benefit of 32% increase in stripper Capacity & Steam reduction by 9%



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INNOVATION 3 STRIPPER REBOILER

STRIPPER REBOILER



• PROBLEM STATEMENT

Stripper reboiler PHE leaking frequently because of Acidic environment at a Operating temperature of 150 C.

PHE unable to replace with Shell and Tube heat exchanger due to 1.Less delta T

• Limitation in condensing the stripper vapor

2.Space constraint.



STRIPPER REBOILER



• LOSSES

Gasket replacement once in six months

Loss of material & Loss of steam due to Gasket leaks



WHY? WHY? ANALYSIS FOR FREQUENT REBOILER LEAKING





PROJECT SAVINGS

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GHG INVENTORISATION





APPROACH & INITIATIVES

- Planning to replace grid power by solar power
- Adopted various energy conservation measures to reduce the steam and Power consumptions
- Exploring Biomass based boiler for future expansion.



50% Renewable Energy by 2030

AWARDS & RECOGNIZATIONS























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- 2004 EXCELLENT ENERGY EFFICIENT UNIT
- 2005 INNOVATIVE PROJECT & MOST USEFUL PRESENTATION AWARD
- 2006 INNOVATIVE PROJECT AWARD
- 2007 EXCELLENT ENERGY EFFICEICENT UNIT
- 2008 EXCELLENT ENERGY EFFICIENT UNIT
- 2011 ENERGY EFFICIENT UNIT
 - 2011 ENVIRONMENTAL BEST PRACTISE
- 2012 INNOVATIVE PROJECT AWARD
- 2012 EXCELLENT ENERGY EFFICIENT UNIT
- 2015 ENERGY EFFICIENT UNIT
- 2021 FCCI AWARD

THANK YOU